







# ENABLING HIGH-ENERGY/HIGH-VOLTAGE LITHIUM-ION CELLS FOR TRANSPORTATION: THEORY AND MODELING

**Project ID: BAT253** 

#### **HAKIM IDDIR**

Argonne National Laboratory
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2018 DOE Vehicle Technologies Office Annual Merit Review

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# **OVERVIEW**

### **Timeline**

■ Start: October 1, 2014

■ End: Sept. 30, 2018

■ Percent complete: 94%

# **Budget**

- Total project funding: FY17 \$4.0M
- BAT252, BAT253, and BAT254 (ANL, NREL, ORNL, LBNL)

### **Barriers**

- Development of PHEV and EV batteries that meet or exceed DOE and USABC goals
  - Cost
  - Performance
  - Safety

### **Partners**

- Oak Ridge National Laboratory
- National Renewable Energy Laboratory
- Lawrence Berkeley National Laboratory
- Argonne National Laboratory









### PROJECT OBJECTIVES - RELEVANCE

Gain understanding of the atomic-scale processes that influence the structure and stability of NMC surfaces under various electrochemical environments

### **MILESTONES**

- Determination of surface structures and the driving force for surface elemental segregation
- Theoretical predictions of electrolyte and additive-NMC surface interactions
- Theoretical predictions of electrolyte decomposition and dissolution products
- Understanding of coating structures, surface reconstructions, and influence on elemental segregation



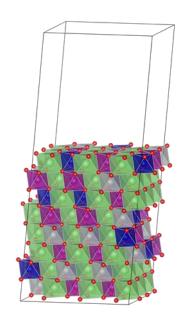






# APPROACH ATOMISTIC MODELING

- Spin-polarized density functional theory (DFT)
- Generalized gradient approximation (GGA) parametrized by Perdew, Burke, and Ernzerholf (PBE).
- The GGA+U scheme is used for applying the on-site correlation effects among 3d electrons of the transition metals (TM)
- After geometry optimizations within the DFT+U framework, electronic relaxation was performed using a single point calculation with the hybrid functional HSE06
- Bulk solvent effects were accounted for by using an implicit solvation (VASPsol)
- Calculations in solution were performed using Gaussian09 with the M062X functional, 6-311+G(d,p) basis set and the CPCM solvent model



Periodic boundary conditions (slab models)

#### **ELECTROCHEMICAL MODELING**

- In general, the electrochemical modeling activities build on earlier successful characterization and modeling studies in extending efforts to high-energy and high-voltage lithium ion systems.
  - Present focus is on electrode side reactions and crosstalk between electrodes.





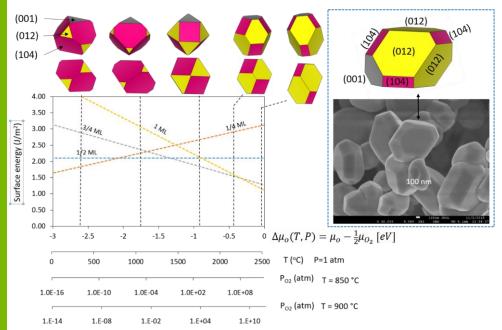


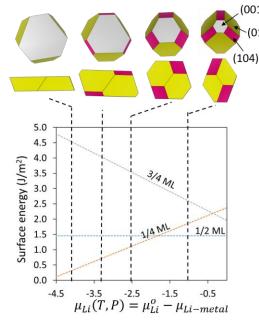


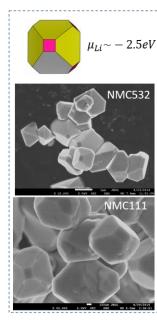
#### MOST RELEVANT NMC FACETS

Surface energy of (012) facet as a function of the oxygen chemical potential (NMC111)

Surface energy of the (001) facet as a function of the Li chemical potential (NMC111)







G. Chen et al. (LBNL)

- The (012) surface is predominant (>80% of total surface area)
- This facet is used as the prototype surface in our models

Predicted particle shapes, surface activity and stability verified by experiments









# SYNTHESIS OF SURFACE-SPECIFIC NMC SINGLE CRYSTALS G. Chen et al. (LBNL)

100 (-1 -1 4) (012) (0 0 1) (001) 80 (0 -1 -4) (104) (104) 1 Jun JEOL 8/11/2016 5.0KV SEI SEM NO 8.0mm 4:44:54 (-1 1 2) Percent Percent 100 nm 100 nm 20 Octahedron T-octahedron Polyhedron **Platelet** (-1 -1 4) (-1 0 2) 100 nm (0 0 1) (-1 1 2)  $(0\ 0\ 1)$ (0 -1 -2)



um



(0 -1 -4)

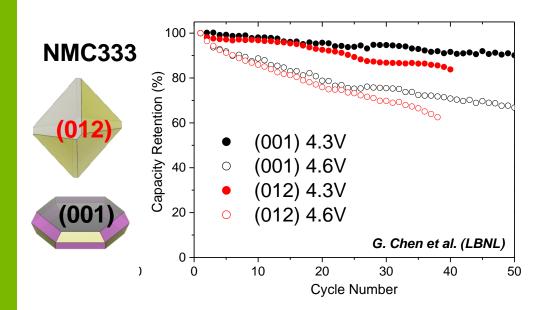
(104)

(1 - 1 - 4)





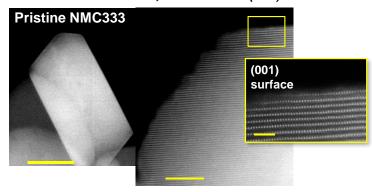
#### **EXPERIMENT CONFIRMS PREDICTED TRENDS**

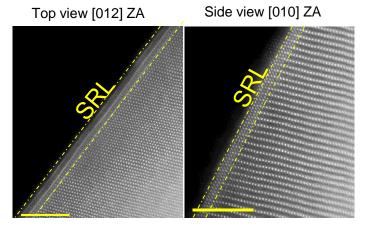


- Same composition (NMC333), same size (~200 nm) and same voltage window.
- Sample with (012) surface outperforms (001) surface in initial capacity but (001) sample has better cycling stability.

Pristine NMC has surface-dependent surface reconstruction layers (SRL)







- Typical surface reconstruction layer (SRL) on pristine NMC333 is ~1 nm.
- Formation of SRL facet dependent no SRL seen on pristine (001) surface of NMC333.

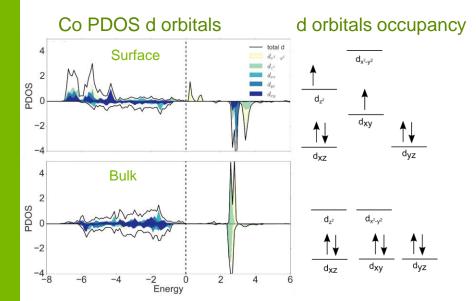




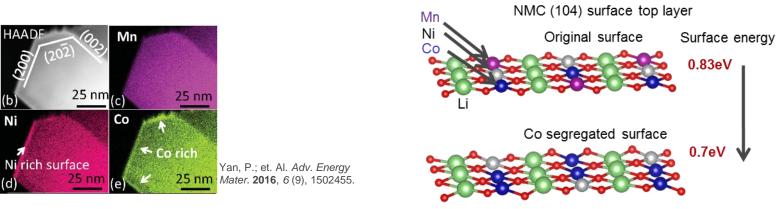




### Co SURFACE SEGREGATION TO (104) FACET



- Bulk: unoccupied states and the magnetization is zero, indicating Co<sup>3+</sup> in the low spin configuration.
- The crystal field splitting energy is less than the spin pairing energy (P) → the low spin configuration is favored.
- Surface: magnetization, Bader charges, and PDOS analysis indicates Co<sup>3+</sup> in an intermediate spin state.
- The crystal field splitting energy < P</li>



The stability of intermediate spin state Co ions at the (104) NMC111 surface produces a thermodynamic driving force for segregation

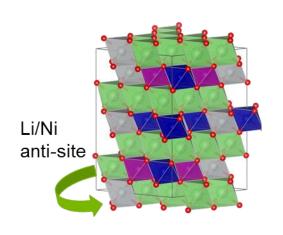


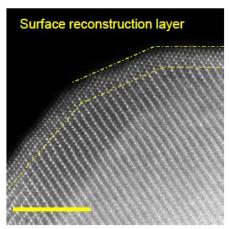






#### **FACET-DEPENDENT NI SEGREGATION**

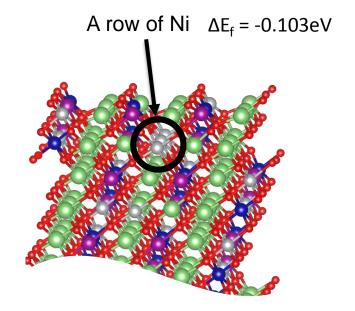




■ Bulk Li/Ni anti-site defect formation energy is  $E_f \approx 0.3 eV \rightarrow$  equilibrium concentration:

$$C = N_{conf} e^{\frac{-E_f}{RT}}$$
  $\rightarrow$  1.3% @ T = 298.15 K

- The anti-site defect formation energy is independent on its distance to the surface
- The formation energy of a row of anti-site defect near the surface is slightly negative



- There is a driving force to form a spinel-like top layer in the fully lithiated (012) NMC111 surface -
- The results suggest a mechanism for Ni migration and phase transformation near the surface

Li-Ni exchange and Ni migration to the surface is at the origin of the surface reconstruction



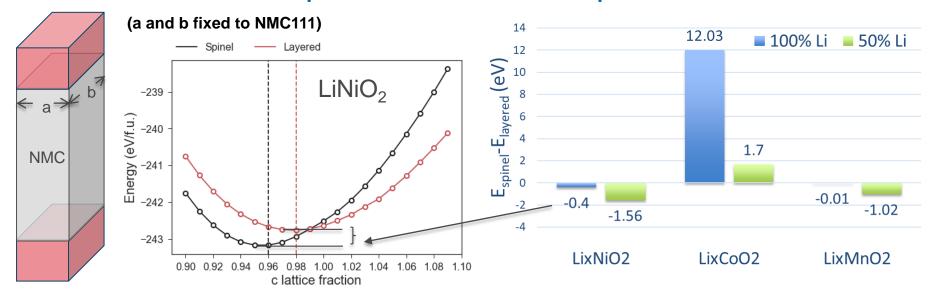




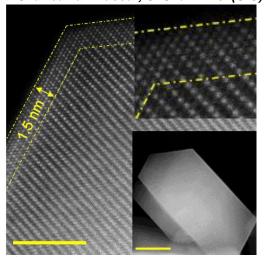


# STRAIN DRIVEN SPINEL STABILIZATION AT THE (012) SURFACE

#### The reconstructed surface is pinned to the unit cell of the particle



#### R. Shahbazian-Yassar, S. Sharifi Asl (UIC)



- LiNiO<sub>2</sub> and LiMnO<sub>2</sub> spinel-like phases are more stable than the layered phases when the phase is pinned to the NMC lattice.
- More Li-Ni exchange than Li-Mn exchange → Ni-rich surface reconstruction.

There is a driving force for Ni to segregate to the surface and reconstruct to a spinel-like phase



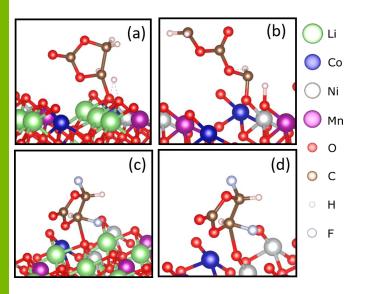


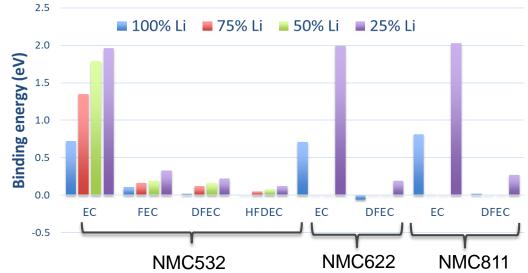




# FLUORINATED VS NON-FLUORINATED ELECTROLYTES

See BAT252





- (a) EC on a lithiated (012) surface
- (b) EC on a delithiated (012) surface
- (c) DFEC on a lithiated (012) surface.
- (d) DFEC on a delithiated (012) surface.

EC oxidation  $\Delta E_b = -2.3eV$ 

DFEC oxidation is not favorable

- Fluorinated compositions: FEC, DFEC and HFDEC present weaker interactions with the NMC surfaces.
- Adsorption/reaction energies of fluorinated molecules are much smaller than that for EC → less decomposition of fluorinated compositions is expected. EC would decompose preferentially, since it competes favorably for the adsorption sites.
- The trend in binding energies is independent of Ni content in the transition metal layer

Limited cathode surface reconstructions/transformations are expected with the fluorinated electrolytes compared to the non-fluorinated electrolytes



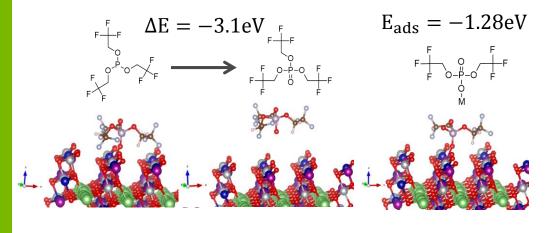




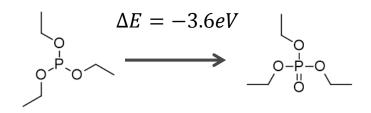


# NMC SURFACE-PHOSPHITE ADDITIVES INTERACTION

See BAT252



- CH<sub>2</sub>CF<sub>3</sub> groups of TTFP do not impede
   P-O interaction at the surface
- The molecule is easily oxidized to TMSPa
- If TTFP loses a CH<sub>2</sub>CF<sub>3</sub> group the product is stable at the surface.



- TEPi is oxidized to TEPa at the surface.
- No stable species at the surface (no surface passivation)

The strength of the interaction depends on the functional groups in the phosphite an the degree of decomposition of the additive

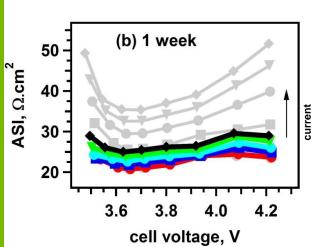








### AGING OF TMSPI MITIGATES IMPEDANCE RISE



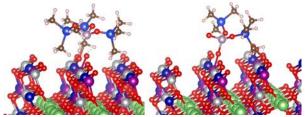
- Electrolyte:
   Gen2
  1 wt% PX<sub>3</sub>
   fresh
   1 week

  10μΑ

  10μ
- ASI plot for aged (1 week) electrolyte containing 1 wt% TMSPi (color lines).
- The grey lines indicate the baseline electrolyte tested using identical cycling and HPPC protocols.
- Current vs. time potentiostatic hold at 4.6 V vs Li/Li<sup>+.</sup>
- Baseline electrolyte (black line) 1 wt% PX<sub>3</sub> before (blue line) and after one week of exsitu aging (red line).
- 1 week old →lowest oxidation current

#### See BAT252

- TMSPi interaction with the surface is weak due to bulky TMS groups
- TMSPi can lose a TMS group and form a phosphate on the surface
- The phosphate adsorbs favorably on the surface



**Increasing Stability** 

# TMSPi decomposition products passivate the surface









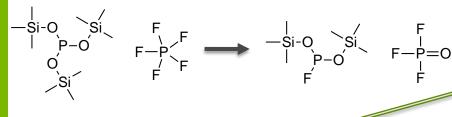
See BAT252

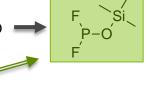
E = 0.0eV

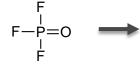
E = -1.0eV

E = -1.8eV

E = -2.5eV

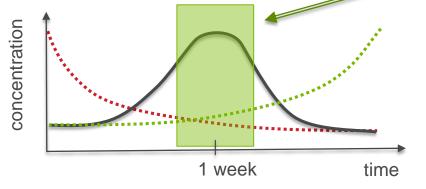


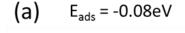


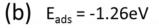


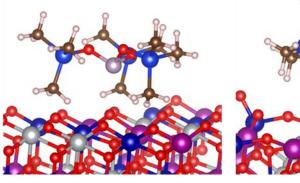


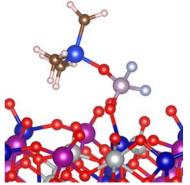












- TMSPi decomposition to PF<sub>3</sub> route is favorable.
- Reaction with PF<sub>5</sub> is favored after the first decomposition step (first reaction step with HF is more favorable than with PF<sub>5</sub>).

Surface passivation by the partially decomposed TMSPi Molecular configuration for chemisorbed (a) PX3 and (b) PF2X molecules on partially delithiated NMC.

TMSPi (PX<sub>3</sub>) has a weak interaction with the surface while PF<sub>2</sub>X (1 branch) molecules interact strongly with the surface (chemisorption, surface passivation).

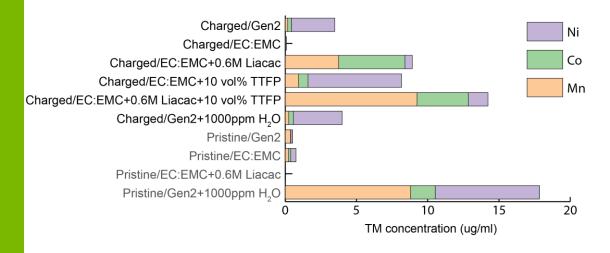








See BAT252



Transition metal dissolution in the absence of LiACAC

- In the charged state, Ni cations are first to be reduced → More Ni dissolution in charged state.
- In the pristine state, Mn cations are first to be reduced → More Mn dissolution in pristine state.

Decomposes

Mn-oxo complex intermediates contribute to Mn dissolution without oxidation of the solvent

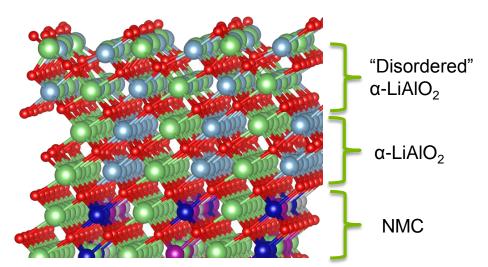


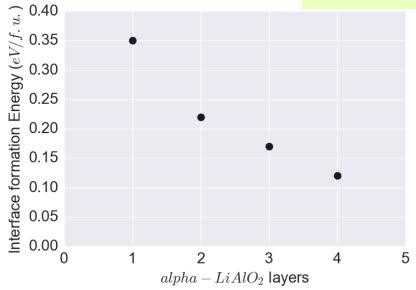






- α-LiAlO2 / NMC interface formation energy is very low ~ 0.1eV/f.u.
- γ-LiAlO2 / NMC does not form a simple interface (symmetry considerations).





 $Interface\ Energy = E_{LiAIO2\_slab} + E_{NMC\_Bulk} - E_{LiAIO2/NMC}$ 

- α-LiAlO2 / "disordered-α-LiAlO2" interface makes the α-LiAlO2 /NMC less favorable.
- 4 α-LiAlO2 layers or more compensates the effect of the disordered phase.

A thin buffer α-LiAlO<sub>2</sub> phase between γ-LiAlO<sub>2</sub> and NMC (012) surface is predicted



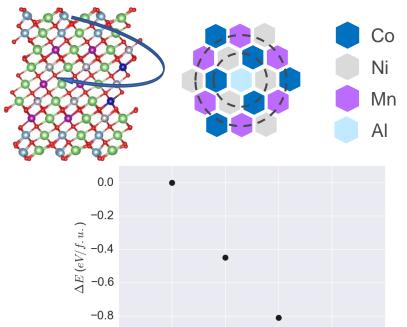




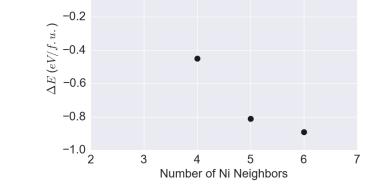


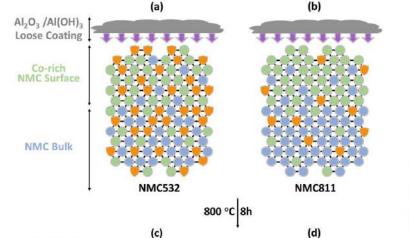
#### **ALUMINA EFFECT ON METAL SEGREGATION**

#### See BAT254



Specie swapped	$AIO_2/NMC111$ $\Delta E (eV)$	LiAlO <sub>2</sub> /NMC111 ΔE (eV)	$AIO_2/Li(M)O_2$ $\Delta E (eV)$
Со	1.63	-0.02	0.95
Ni	0.21	-0.33	0.03
Mn	-1.02	0.42	-0.52



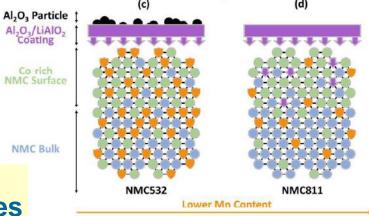


- Swapping Ni and Co in the TM layer changes the Al environment.
- Energy gain with increasing Ni and Co near surface Al is larger than the cost of the exchange (Mn-Al swapping).
- Al prefers to be surrounded by Ni then Co but not Mn.

The energy decreases when the number of Ni neighbors to Al increases







More Al Insertion





#### **SUMMARY**

#### **Atomistic modeling**

- Thermodynamic model predicts particle shape, (012) surface most reactive facet, facetdependent transition metal segregation
- Fluorinated electrolytes present a lower reactivity toward oxidation at the cathode compared to non-fluorinated electrolytes.
- The strength of the interaction of phosphite additives with the cathode surface depends on the functional groups and the degree of decomposition of the additive.
- TMSPi decomposition products passivate the surface of NMC cathodes.
- Complexation of transition metals affects dissolution.
- A thin buffer α-LiAlO<sub>2</sub> phase between γ-LiAlO<sub>2</sub> and NMC (012) surface is predicted.
- Al dissolved in the cathode induces elemental segregation to the surface.

#### **Electrochemical modeling**

- Simple electrode current balance model effective for examining a wide range of cell characteristics affected by side reaction phenomena.
- Existing electrochemical model modified to examine side reactions and crosstalk between electrodes.
- The long time constant for cell current change observed during high voltage potentiostatic holds is generally associated with side reactions. Similarly, most of current goes into the redox of side reactants and not lithium loss.









#### **FUTURE WORK AND WORK IN PROGRESS**

#### **Atomistic modeling**

- Surface dopants to mitigate dissolution, surface reconstruction, reaction with the electrolyte (descriptors?).
- Surface reconstruction-strain-segregation relationships.
- Effect of surface reconstructions on impedance raise.
- Additional additives-surfaces interactions.
- Solvent and additives decomposition micro-kinetics modeling.

#### **Electrochemical modeling**

- Expand model to include impact of transition metal dissolution, oxygen release from oxide surface, and gas generation within cell.
- As side reaction complexity increases, methods for simplifying electrochemical model will be explored.









#### CONTRIBUTORS AND ACKNOWLEDGMENT

#### **Research Facilities**

- Materials Engineering Research Facility (MERF)
- Post-Test Facility (PTF)
- Cell Analysis, Modeling, and Prototyping (CAMP)
- Battery Manufacturing Facility (BMF)
- Advanced Photon Source (APS)
- Argonne Leadership Computing Facility (ALCF)

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#### RESPONSE TO PREVIOUS YEAR'S REVIEWER COMMENTS

#### All comments by reviewers were positive last year

- This reviewer praised the approach as excellent. The reviewer pointed out the modeling efforts are combined with experimental studies. The obtained models are used to understand the interactions between cathode surface and electrolyte/additives and the reviewer concluded the results are consistent with the experimental findings and surface analysis.
- The reviewer praised this work for achieving very impressive milestones. The project has had a significant progress in one year the reviewer observed, and the findings can be used as a predictive tool to improve high-energy LIBs.
- This reviewer said excellent collaboration with other teams was evident and needed. The strength(s) of each collaborator was maximized.
- The reviewer acknowledged that the project is very helpful in order to understand electrode bulk and surface structures, processes at surfaces and interfaces, and electrolyte-surface interactions to address the problems associated with "enabling" high-energy Li-ion cells.
- The reviewer pointed out this work can be improved by providing more experimental support for the computational results.

**Response** – We thank the reviewers for their encouraging remarks on the progress made within the project and will endeavor to incorporate as much experimental collaboration as possible.





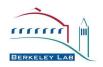




# TECHNICAL BACKUP SLIDES









# Simple Electrode Current Balance Model Utilized to Make **Basic Conclusions about Side Reactions**

For each electrode, the rate of change in capacity ( $C_{\perp}$  and  $C_{\perp}$ ) combined with side reaction current ( $I_{Oxd}$  for positive and  $I_{Red}$  for negative) is equal to the cell current ( $I_{Cell}$ ).

$$I_{Cell} = \frac{dC_{+}}{dt} - I_{Oxd} = -\left(\frac{dC_{-}}{dt} + I_{Red}\right) \qquad C_{Cell} = C_{+} + C_{-}$$

$$\frac{dC_{Cell}}{dt} = I_{Oxd} - I_{Red}$$

Positive oxidation side reactions increase cathode capacity  $\frac{dC_{Cell}}{dt} = I_{Oxd} - I_{Red}$  (C<sub>+</sub>) and negative reduction side reactions decrease anode capacity (C\_).

$$CE = \frac{I_D}{I_C} \frac{I_C - (I_{Red})_{Cavg}}{I_D + (I_{Red})_{Davg}}$$

 $CE = \frac{I_D}{I_C} \frac{I_C - (I_{Red})_{Cavg}}{I_D + (I_{Red})_{Davg}}$ • If the discharged cell's anode is empty, then the current efficiency (CE) is determined by the arrow. efficiency (CE) is determined by the cycling currents ( $I_C$  for charge and  $I_D$  for discharge) and the side reduction current.

$$CE = \frac{I_D}{I_C} \frac{I_C - (I_{Oxd})_{Cavg}}{I_D + (I_{Oxd})_{Davg}}$$

If the discharged cell's anode contains excess lithium, then the current efficiency is determined by the cycling currents and the side oxidation current.

$$I_{Cell} = -I_{Oxd}$$

 Cell current for NMC//Graphite cells at long times during a potentiostatic hold is equal to the positive oxidation side reaction current, assuming the graphite electrode is in a twophase region (i.e. flat OCV curve).



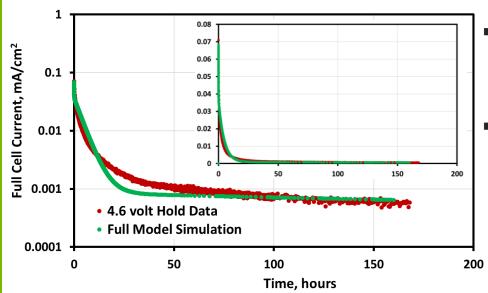




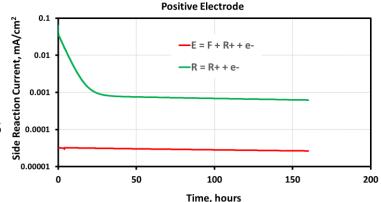


# Electrochemical Model Used to Examine Potentiostatic Hold Data on Full Cells

### 4.6 volt hold on NMC//graphite coin cell at room temperature



- Time constants associated with the main cell reaction are on the order of hours or less.
- The long time constant for the hold is generally associated with side reactions.
  - Slow change in R and R+ concentrations.
  - SEI (i.e. F) growth on the positive.
- Multiple side reactions needed to improve fit.
- SEI generation reactions at least an order of magnitude lower than main crosstalk reactions.
- Most of current goes into redox of side reactants (i.e. R crosstalk reactions) and not lithium loss.
- Corresponding small change in cyclable lithium.







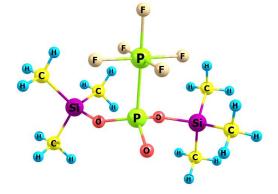




# TMSPI DECOMPOSITION

$$Li^{\dagger}$$
 F F  $H_2O$  F F H-F  $Li-OH$ 

Stable intermediate



- The actual decomposition mechanism may involve HF and PF<sub>5</sub>.
- Intermediates have been found experimentally (NMR) and theoretically (DFT).









# TMSPI DECOMPOSITION TIMELINE

$$E = 0.0eV$$

$$E = -0.15eV$$

$$E = -0.25eV$$

$$E = -0.58eV$$

- TMSPi reaction with HF is thermodynamically favorable.
- Further decomposition goes trough PF<sub>3</sub> route preferentially.
- Reaction with PF<sub>5</sub> is favored after the first decomposition step.

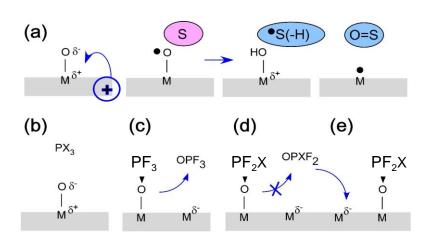




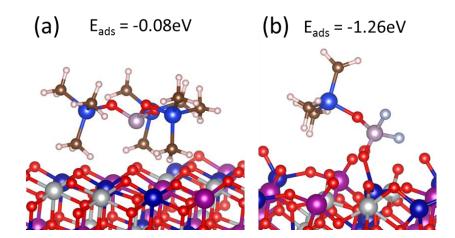




#### SURFACE PASSIVATION MECHANISM



- (a) oxidation of the solvent by charged M-O reaction centers on the cathode surface
- (b) No interaction.
- (c) PF<sub>3</sub> oxidation via oxygen removal from the surface.
- (d-e) PF<sub>2</sub>X binds to the surface.



Molecular configuration for chemisorbed (a) PX3 and (b) PF2X molecules on partially delithiated NMC.

- The phosphate formed at the surface is less prone to lose a OTMS group.
- TMSPi (PX<sub>3</sub>) has a weak interaction with the surface while PF<sub>2</sub>X (1 branch) molecules interact strongly with the surface (chemisorption, surface passivation).









# **Methodology for Electrochemical Model**

# Combines thermodynamic and interfacial effects with continuum based transport equations

# Bulk Solid-State Diffusion

$$\frac{\partial c_{Sb}}{\partial t} = \frac{\partial}{\partial z} \left( D_{Sb} \frac{\partial c_{Sb}}{\partial z} \right)$$

Transport, Reaction, and SEI Growth of Side Reaction Components  $i_{n} = i_{0} \left\{ \exp \left[ \frac{\alpha_{A}F}{RT} (\Phi_{1} - \Phi_{2} - U - \eta_{c}) \right] - \exp \left[ -\frac{\alpha_{C}F}{RT} (\Phi_{1} - \Phi_{2} - U - \eta_{c}) \right] \right\}$   $\frac{\sum_{i} i_{n}}{z_{i}F} = -D_{i} \frac{c_{iE} - c_{iS}}{\delta_{SEI}} \qquad \eta_{c} = \frac{RT}{nF} \sum_{i} s_{i} \ln \frac{c_{iE}}{c_{iS}} \qquad \sum_{i} s_{i} M_{i}^{z_{i}} \leftrightarrow ne^{-}$   $\frac{d\delta_{SEI}}{dt} = \frac{\sum_{i} i_{n} V_{SEI}}{F} \qquad \qquad \frac{\partial \varepsilon c_{i}}{\partial t} = \nabla \cdot \left( \frac{\varepsilon D_{i}}{\tau} \nabla c_{i} \right) + a \sum_{i} j_{n}$ 

## Transport through Cell Sandwich

$$\varepsilon \frac{\partial c}{\partial t} = \frac{\varepsilon}{\tau} \frac{\partial}{\partial x} \left( D \frac{\partial c}{\partial x} \right) + \frac{1}{z_{+} \nu_{+} F} \frac{\partial \left[ \left( 1 - c \overline{V}_{e} \right) \left( 1 - t_{+}^{o} \right) i_{2} \right]}{\partial x}$$

$$i_{2} = -\frac{\kappa \varepsilon}{\tau} \frac{\partial \Phi_{2}}{\partial x} - \nu R T \frac{\kappa \varepsilon}{F \tau} \left( \frac{s_{+}}{n \nu_{+}} + \frac{t_{+}^{o}}{z_{+} \nu_{+}} \right) \left( 1 + \frac{\partial \ln f_{\pm}}{\partial \ln c} \right) \frac{1}{c} \frac{\partial c}{\partial x}$$

$$\frac{\partial i_{2}}{\partial x} = F z_{+} \sum_{k} a_{k} j_{kn} \qquad I = i_{1} + i_{2} \qquad i_{1} = -\sigma_{eff} \frac{\partial \Phi_{1}}{\partial x}$$

- Side reaction components diffuse between electrodes and through SEI from electrolyte where they react with electrons diffusing from the solid conductors. Initially the reaction front assumed to be narrow and close to solid.
- All electrolyte components from side reactions are considered minor constituents.
- Volume averaged transport equations account for the composite electrode geometry.
- The system of partial differential equations are solved numerically to obtain concentration, potential, and current distributions throughout cell.

Description of original model in *Journal of The Electrochemical Society*, **155** (8) A603 (2008)









# Initial Electrochemical Model Developed Based on Generic Side Reaction Mechanism

Initial rate limitation (i.e. kinetics, diffusion, or combination) for side reactions based on known or estimated reaction potentials

**Negative:** 
$$xLi^+ + xe^- + \theta \leftrightarrow Li_x\theta$$
 Main electrochemical reaction

E°=0.8v, Diffusion 
$$Li^+ + e^- + E \leftrightarrow SEI$$

E°=2.0v, Diffusion 
$$e^- + R^+ \leftrightarrow R$$

E°=0.2v, Kinetics 
$$Li^+ + e^- + R \leftrightarrow SEI$$

Reduction side reactions

**Positive:** 
$$Li_y\theta \leftrightarrow yLi^+ + ye^- + \theta$$

Main electrochemical reaction

and/or Diffusion 
$$E \leftrightarrow F + R^+ + e^-$$

E<sub>0</sub>=2.0v, Diffusion 
$$R \leftrightarrow R^+ + e^-$$

Oxidation side reactions

- Model includes reduction and oxidation of electrolyte solvent specie (E) and reacted solvent specie (R), as well as crosstalk between electrodes.
- In actuality each side reaction is likely a complex matrix of reactants and products that probably occur over a range of potentials.
  - R is actually  $R_1$ ,  $R_2$ ,  $R_3$ ,...

Description of reaction mechanism in *Journal of The Electrochemical Society*, **164** (2) A508 (2017)







